



<u>REMARKS</u>

In paragraph three of the Office Action, claims 27-39 and 41-60 were rejected under 35 U.S.C. §103(a) as being unpatentable over Sakon et al. (U.S. Patent No. 5,560,857) in view of Stanford et al. (U.S. Patent No. 5,244,000) and Kern (Hand Book of Semiconductor wafer cleaning technology) and further in view of Sehested et al. (J.Phys.Chem.).

In one aspect, the current invention discloses a process wherein ozone in combination with a scavenger removes organic contamination on a substrate. Applicants do not believe that the references alone, or taken in combination, render the claims obvious for at least three reasons.

First, the invention is directed to the removal of organic contaminants resulting from a previous lithographic step rather than directed to the removal of metallic contaminants (which is the subject of the Sakon reference). As discussed in paragraph 4 of the enclosed Declaration of Stefan DeGendt, one of the inventors of the present application, there is a substantial difference between the removal of organic contaminants (and especially the removal of organic contaminants resulting from a previous lithographic step) and the removal of metallic contaminants.

As discussed in paragraph 5 of the enclosed declaration, a typical wet cleaning sequence is SC1 step and then SC2 step. The SC1 step is typically an alkaline oxidizing step, used to remove particles in general, but is prone to introducing metallic contamination, requiring a further process step (e.g., SC2 step). The SC2 step is typically an acid oxidizing step, used to remove metallic species. The cleaning from the SC1 and SC2 steps is surface (monolayer)





cleaning. This cleaning sequence is generally known as an RCA clean and has been introduced by Werner Kern 'RCA Rev. 31, 1970, p.187.

When thicker (visible) layers or residues must be removed, such as a layer of organic photoresist, at least extra processing steps are added. Typically, the sequence is as follows: SPM (sulphuric peroxide mixture) step, then diluted HF step, then SC1 step, and then SC2 step. SPM is a very oxidizing substance which very aggressively removes organic contaminants (such as those caused by a previous lithographic step). The SPM step is typically followed by a step in which diluted HF is applied. After the diluted HF step, the SC1 and SC2 steps are applied to further clean the substrate. The claims currently pending give an alternative to the SPM step. As discussed in the background section of the patent, the SPM step has several disadvantages including: (1) using expensive chemicals; (2) requiring high processing temperatures; and (3) causing serious problems in terms of chemical waste treatment of the sulphuric peroxide mixture. Thus, the present invention avoids the need for using, for example, the caustic substance of the sulphuric peroxide mixture. Instead, a much more environmentally friendly liquid comprised of water, ozone and an additive acting as a scavenger is used, as claimed in claims 27, 51 and 60. See paragraph 8 of Declaration of Stefan DeGendt.

The prior art actually teaches away from the use an SC2 step in a photoresist removal step. For example, the appended article by Werner Kern entitled "The Evolution of Silicon Wafer Cleaning Technology," *J. Electrochem. Soc.*, Vol. 137, June 1990, discusses SC1 and SC2 steps. In the second full paragraph on page 1888, Mr. Kern describes an SC1 step, as shown in the following excerpt:

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In the first treatment step, the wafers are exposed to a hop mixture of waterdiluted hydrogen peroxide and ammonium hydroxide. This procedure was designed to remove organic surface films by oxidative breakdown and dissolution to expose the silicon or oxide surface for concurrent or subsequent decontamination reactions.

Mr. Kern, again on page 1888, third full paragraph, describes an SC2 step, as shown in the following excerpt:

The second treatment step exposes the rinsed wafer to a hot mixture of water-diluted hydrogen peroxide and hydrochloric acid. This procedure was designed to remove alkali ions and cations such as AL⁺³, Fe⁺³, and Mg⁺², that form NH₄OH-insoluble hydroxides in basic solutions.

On page 1888, in the paragraph beginning with "optional processing steps," a preliminary cleanup treatment with a hot SPM is mentioned, as discussed in the following excerpt:

A preliminary clean-up treatment with a hot H₂SO₄-H₂O₂ mixture (2:1 vol) can be used advantageously for grossly contaminated wafers having visible residues, such as photoresist layers.

Mr. Kern concludes that the chemistry of an SC2 step is not for photoresist removal, as discussed on page 1888 (bottom left paragraph):

However, using high-purity and point-of-use ultrafiltered and particle-free HF solution is used under controlled conditions, more harm than good can result. A silicon surface that was exposed to HF is highly reactive and immediately attracts particles and organic contaminants from solution, DI water, and ambient air. Contrary to SC-1, the subsequent SC-2 solution, which has no surfactant activity, will not eliminate these contaminants.

(Emphasis added). Stefan DeGendt, in his declaration, concludes that not every mixture of an inorganic acid (e.g. HCl) and hydrogen peroxide are capable of removing organic contaminants from silicon substrates. See paragraph 7 of Declaration of Stefan DeGendt. Thus, the Kern reference on page 1888 clearly states that the SC2 step will not affect the removal of photoresist.

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Second, the invention calls for the use of ozone rather than the use of hydrogen peroxide (as taught in the Sakon reference). Contrary to the assertion by the Examiner, ozone is not interchangeable with hydrogen peroxide, as discussed in the appended declaration. As an initial matter, ozone is much more environmentally friendly than hydrogen peroxide. See paragraph 9 of Declaration of Stefan DeGendt. Moreover, the reactivity of ozone is much higher than hydrogen peroxide. Specifically, in order to provide the necessary reactivity in a hydrogen peroxide mixture, the concentration of the hydrogen peroxide is typically greater than 10% whereas for the equivalent reactivity in an ozone mixture, the concentration of ozone is in the parts per million (ppm) range. Id. Finally, ozone is much cheaper to use than hydrogen peroxide. As discussed previously, the concentration of hydrogen peroxide must be above a certain percentage in order to achieve the desired reactivity. Over time, use of the bath decreases the concentration of the hydrogen peroxide, requiring the replacement of the bath or the addition of hydrogen peroxide. By contrast, ozone need only be bubbled up in the mixture, making processing significantly easier. Id.

Third, Sakon discloses the use of acetic acid but for an entirely different purpose – not for use as a scavenger, as recited in each of the claims. The Examiner states that the Sakon reference must only teach that the use of acetic acid provides some advantage in the cleaning composition.

Applicants respectfully disagree. A general teaching regarding the benefit of using acetic acid, without more, is an insufficient teaching to those skilled in the art to use acetic acid as a scavenger. Rather, there must be some suggestion to use acetic acid as a scavenger. Clearly, the Sakon reference provides no such teaching and therefore does not render the claims obvious.





Moreover, the Stanford reference is different from the present invention for at least the reasons stated with respect to the Sakon reference.

In paragraph five of the Office Action, claim 49 was provisionally rejected under 35 U.S.C. §101 as claiming the same invention as claim 27 of co-pending Application Serial No. 09/207,546. Applicants have amended claim 27 in co-pending Application Serial No. 09/207,546.

In paragraphs seven and eight of the Office Action, claim 27, 51, and 60 were provisionally rejected under judicially created doctrine of obvious-type double patenting. Upon allowance of claims in the present cases, applicants will submit a terminal disclaimer in the copending case.

CONCLUSION

If for any reason, the application is not considered to be in condition for allowance on the next Office Action and an interview would be helpful to resolve any remaining issues, the Examiner is requested to contact the undersigned attorney at (312) 913-0001.

Respectfully submitted,

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Dated: 9/24/31

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APPENDIX UNDER 37 CFR 1.121(c)

27. (Thrice Amended) A method for removing organic contaminants from a substrate, the organic contaminants resulting from a previous lithographic step, the method comprising the steps of:

contacting at least one side of said substrate with a liquid comprising water, ozone and an additive acting as a scavenger, wherein the proportion of said additive in said liquid is less than 1% molar weight of said liquid; and

maintaining said liquid at a temperature less than the boiling point of said liquid.

51. (Twice Amended) A method for removing organic contaminants from a substrate, the organic contaminants resulting from a previous lithographic step, the method comprising the steps of:

contacting at least one side of said substrate with a liquid comprising water, ozone and an additive acting as a scavenger, wherein said liquid is comprised substantially of water; and maintaining said liquid at a temperature less than the boiling point of said liquid.

60. (Twice Amended) A method for removing organic contaminants from a substrate, the organic contaminants resulting from a previous lithographic step, the method comprising the steps of:

holding said substrate in a tank; and

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filling said tank with a fluid comprising water, ozone and an additive acting as a scavenger, and wherein the fluid is comprised substantially of water.

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The Evolution of Son Wafer Cleaning Techlogy

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ABSTRACT

The purity of water surfaces is an examinal requisite for the successful fabrication of VLSI and ULSI silicon circuits. Water cleaning chemistry has remained essentially unchanged in the past 25 years and is based on hot alkaline and acidic hydrogen peroxide solutions, a process known as "BCA Standard Clean." This is still the primary method used in the industry. What has changed is its implementation with optimized squipment: from simple immersion to containing approxing, megasonic techniques, and enclosed system processing that allow simultaneous removal of both contaminant films and particles. Improvements in water drying by use of inopropensal squar or by "slow-pull" out of hot described water are being investigated. Several attendance cleaning methods are also being tested, including choline solutions, obtained vapor exching, and UV/azone treatments. The evolution of alligon water cleaning processes and exchanges is exceed and reviewed from the 1950s to August 1989.

The importance of clean substrate surfaces in the fabrication of seminonductor microelectronic devices has been recognized since the early days of the 1950s. As the requirements for increased device performance and reliability have become more stringent in the era of VLSI and ULSI silicon circuit technology, techniques to avoid confaces have become critically important. Besides, over 50% of vield losses in integrated circuit raprication are generally accepted to be due to microcontamination. Trace impurities, such as nodium ions, metals, and particles, are especially detrimental if present on acmicanductor surfaces during high-temperature processing (thermal oxidation, diffusion, opitoxial growth because they may spread and diffuse into the semiconductor interior. Impurities must also be removed from surfaces before and/or after lower temperature steps, such as chemical vapor deposition, depant implanting, and plasma reactions. Postcleaning after photoresist stripping is necessary for every mask level throughout the production process.

Many water cleaning techniques have been tested and several are being used. The generally most successful approach for silicon waters without metallization uses were chemical treatments based on hydrogen peroxide chemistry. This process has remained essentially unchanged during the past 25 years, but important advances have been made in its technical implementation. The evolution of the departing technology for presentallized cilicon waters from its beginning to the present time will be traced in this paper.

Type. Origin, and Effects of Contominants

Impurities on silicon wafer surfaces occur in essentially three forms: (i) contaminant films. (ii) discrete particles, and (iii) adsorbed gases that are of little practical consequence in wafer processing. Surface contaminant films and particles can be classified as molecular compounds, ionic materials, and atomic species. Molecular compounds are mostly particles or films of condensed organic supporterm lubricants, greater, photocraft, solvent radiduce, components from plastic storage containers, and metal capitals or hydroxides. Ionic materials comprise cations and anions, mostly from inorganic compounds that may be physically adsorbed or chemically banded (chemisorbed), such as sodium ions, fluoride ions, and chlorine ions. Atomic or elemental species comprise matals, such as gold and copper, that may be electrochemically plated out on the silicon surface from HF-containing solutions, or they equipment.

The sources of impurities are manifold. In the case of particles, which can be detected and measured much more casily than companient films, the insign sources are equipment, chemicale, factory personnel, and production processes. For example, mechanical equipment, process operators, furnace tubes, film deposition systems, gas piping,

and liquid containers are especially serious acurers, whereas materials, liquid and gresous chemicals, and ambient air tend to cause less particle contamination; but all contribute significantly to the generation of contaminant films. Static charge built up on waters and carriers is a powerful mechanism of particle deposition, but is often overhooked and not properly dealt with.

Molecular contaminant films on water surfaces can mask effective displing of rinsing, cause poor adhesion of deposited layers, and lead to harmful decomposition products. For example, organic films, if heated to high tampera-tures in a nonoxidizing atmosphere, can carbonize and form silicon carbide that can nucleate polycrystalline regious in an epitaxial deposit. Ionic films and metals cause a host of problems in semiconductor devices. During hightemperature processing or on application of an electric field they may diffuse into the bulk of the semicanductor structure or spread on the surface, leading to electrical defacts, device degradation, and yield losses. For example, highly mobile alicali ions may cause drift currents and unstable surface potential, thifts in threshold and flatband voltages, surface current leakage, and may lower the oxide breakdown field of thermally grown layers. In the growth of spitaxial silicon layers, sufficiently high concentrations of lone can give rise to twining dislocations, stacking faults, and other crystal defects. Atomic metals, especially the heavy metals, con affect minerity-carrier lifetime, surface conduction, electrical device stability, and lead to structural defects in opitudal layors. Particles may cause blocking in photolithography and exching or mixing, and load to shorts if they are conductive and located adjacent to conductor lines. They are considered potential killer de-facts if their size exceeds one tenth of the linewidth. Particles that are present during film growth or deposition may lead to pinholes, meterial voids, cracks, and the generation of defects noted above depending on their chemical conposition. Additional information on the nature, origin, datection, and effects of contaminants is available from selected papers and reviews (1-18).

Early Cleaning Procedures

During the early stages of silicon wafer processing until about 1970, one used organic solvent extraction, builing nitric acid, agus regis, concentrated hydrofluoris and, and hot acid inturures as cleaning chemicals. Mintures of sulture and chromic and led to chromium contamination and caused ecological problems of disposal. Mintures of sulfuric acid and hydrogen percented coulor contamination. Aquenus solutions containing hydrogen percented had long been used for cleaning electron tube components (14, 15) but not for camioenducture. In general, impurity levels and particles in process chemicals were high and in themselves tended to lead to surface contamination. Particulate impurities were removed by ultrasonic treatment in detergant solutions or by bruth ortubing. The first caused frequent wafer breakage and the second often deposited more debris from the bristles than it removed from the wafer surfaces.

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Cleaning Processes Based on Hydrogen Peroxide Solutions

Cleaning chemistry.—The first systematically developed cleaning process for bare or oxidized silinan wafers was based on a two-step axidizing and complexing treatment with hydrogen peroxide solutions: (i) an elicalize mixture at high pH followed by (ii) an axidiz mixture at low pH (1). The choice of chemicals was based on reaction chemistry, oxidation potentials, reagent purity, reagent volatility, safety, and economy. The process was developed at RCA, introduced to device production in 1865, and published in 1860 (2)

In the arst treatment step the waters are exposed to a hot mixture of water-diluted hydrogen peroxide and attempolium hydroxide. This procedure was designed to remove organic surface films by oxidative breakdown and dissolution to expose the allient or oxide surface for concurrent or subsequent decontamination reactions. Group DS and DB metals and several other metals, including gold, silver, copper, nickel, cadmium, sinc, cobalt and chromium, are dissolved and removed by the complexing effectiveness of ammonium hydroxide; copper, for example, forms the Cunnill, 12 amino-complex.

The second treatment step exposes the rivid wafer to a hot mixture of water-diluted hydrogen peroxide and hydrochloric and. This procedure was designed to remove climit ions, and cations such as Al⁻¹, Fe⁻¹, and Mg⁻¹, that form NH₂OH-insoluble hydroxides in banks colutions. This accord step also eliminates metallic contaminants that were not entirely removed by the first treatment, such as gold. Electrochemical displacement replaying of heavy metals from the solution is provented by formation of soluble complemes with the dissolved metal ions.

Solution composition, process conditions, and effectiveness.—The solution compositions are based on ultrafiltered deionized water, electronic grade NH₂OH (29 weight percent (w/o) as NH₂), electronic-grade HCl (37 w/o), and high-purity "unstabilized" H₂O₃ (30%). The hydrogen percent must be low in aluminum and stabilizer additives (sodium phosphate, sodium stannate, or amine derivatives) to prevent weight recontamination. The usual volume ratios for the solution used in the first treatment step are 5 H₂O:1 H₂O:1 NH₂OH. the maxime is known as "RCA standard clean 1 or SC-1." The usual volume ratios for the second solution are 6 H₂O:1 H₂O:1 HCl. "RCA standard clean 2, or SC-2." Treatments by the original immersion technique are typically 10 min at 75°-80°C in each solution. Migher temperatures must be evolved to minimize occusive thermal decomposition of the hydrogen percende Intermediate and final rinses in ultrafiltered deionized water are used.

The effectiveness of the process was demonstrated by sensitive radioactive tracer measurements with several redioactive radio process and the expectance-voltage him temperature measurements of MOS capcitors (1). H₂O₃ solutions are unstable at clavated temperature, especially at high pH, rapidly decomposing to H₂O and O₃. The processing temperature should therefore be kept at 75° 80°C to sufficiently activate the mixtures without causing excessively fast decomposition.

Optional processing steps.—A preliminary clean-up treatment with a hot H₂SO₂-H₂O₂ mixture (3:1 vol) can be used advantageously for grossly contaminated waters having visible residues, such as photocentri layers. Another step, not noted in the original paper (1), concerns an etch in HT solution for bare silicon waters, since the hydrous code film from the SC-1 restment may trap trace impurities, its removal before the SC-2 step should be beneficial. A 13s immersion in 1% HT-H₂O solution is sufficient to remove this film, as evidenced by the chance from the hydrophilic oxidized surface to hydrophobic after stripping. However, unless high-putity and point-of-use ultraflitured and particle-free HT solution is used under controlled conditions, more harm than good can result. A silicon surface that was exposed to HT is highly reactive and immediate that was exposed to HT is highly reactive and immediators than solutions. DI water, and the ambient sir. Contrary to SC-1, the

subsequent SC-2 solution, which has no juristiant activity, will not aliminate these contaminants. It may therefore be preferable to rely on the dissolution act on of SC-1 that dissolves and regrows the hydrated oxide layer at about the same rate. If the precisan is used, then the IW HF step prior to SC-1 is acceptable since SC-1 will remove the contaminants. Exposure of bare silicon water to HF after SC-2 should not be done since it would destroy the passivated surface resulting from SC-2 and cause recontamination.

Immersion icchnique.—The original RC i cleaning process was based on a simple immersion teo trique. Several different and improved techniques have been introduced over the years, as will be discussed. The immersion procedure is done in vessels of fissed silica to pre'ent leaching of aluminum, boron, and alkalis if Pyrcx g ass is used. A batch of waters is immersed in the SC-1 o: SC-2 solution under the prescribed conditions. The reaction is terminated by overflow quenching with cold IV water before the waters are transferred to a flow rings system with ultrasitered DI water, followed by spin drying it a water centrifuge. Several types of refined wet bench immersion systems for automated processing are now available for large-scale production (17-19).

Contrifugal spray cleaning.—In 1878, Fill Corporation introduced the first contribued spray electing machine specifically designed for automatic operation with corrective chemicals. The welcar rotate past as attenary spray solution. Placed acids and reagent solutions, including hot SC-1, SC-2, and DI water, are pressure led into a mixing manifold and then directed as a dispersed spray onto the spinning waters. The spin-rinsed waters are desired by high-speed spinning in heated ninogen. An duced volume of freshly mixed reagents is used and the process is faster than by immersion. The chemical cleaning efficiency, according to FSI, is comparable with that of immersion, but particles are removed more afficiently. Improved versions of this system (80) and other types of spray processing machines (17-19) are widely used but tend to require considerable maintenance.

Megamenia cleaning. The original objective of the BCA cleaning process was the removal of contaminant films
rather than particles. To complement this echnique, the magesanic particle removal system was dev sloped at RCA and first described in 1975 (31), A highly emicure noncontact scribbing action on both front and book aide surfaces of the waters is achieved by ultrahigh-fri quency sanic energy while the waters are submerged in it is cleaning so-lution. The sonic waves of 680-800 kHz are generated by an array of piesoelectric transducare. Particles: anging in size from several micrometris down to about 0.5 µm can be efficiently removed with input power densitie : of 2-5 W/cm*. For comparison, ultrasonic systems operate typically at 20-80 kHz and require power densities of t.p to 50 times that of the merasonic system but are much less effective for removing very small particles. Magas into cleaning made it possible to remove simultaneously contaminant films and particles in one operation by comi ining the peroxide treatments with megasonics. The sys am allows moval of particles, organic contaminant file s, and lightly adsorbed contaminants with diluted BC1 salution at the ambient bath temperature of only 35°42°C. Chemisorbed inorganics generally require higher temperatures (about 70°C) for complete description with SC1 and SC2, but no quantitative data are available as yet. A dott iled paper on megasonic water cleaning was published in 1985 (22), Improved messeonic systems built under liner se from RCA have become available in the past few years from Verteq, Semiconductor Technology, and Estek.

Closed system chemical closning.—A system termed Pull-Flow—, developed in 1988 by CFM Ted inclosing, Incorporated, is based on keeping the waters stationary and enclosed in the system during the entire classing, rinsing, and drying process (38). The vessel contains up the waters is hydreulically controlled to remain filled with hot or cold process fluids, including SC-1 and SC-2, that flow sequentially and continuously over stationary waf its loaded in

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المناونات cassettes. The repeated crossing through the phese boundaries in the immersion techniques is thereby climinated. The system thus avoids recontemination problems encountered when waters are pulled out from a

Chronological Literature Survey

Beginning in 1972, independent investigators examined and verified by various analytical methods the effective ness of the RCA cleaning snethed published in 1870 (1). This section chronologically reviews references on discon water cleaning pertaining specifically to hydrogen percuide solutions, up to mid-1889.

In 1972 Handarson published results on the evaluation of SC-1/SC-2 cleaning, using high-energy electron diffraction and Auger electron spectroscopy as melytical methsee is well suited for ods (24). He sunshaded that the prewater cleaning prior to high-temperature treatments, as long as quartz ware is used for processing, as specified by us (1). An additional times such in HF solution after SC-1/ SC-2 caused carbon contamination and nurtice roughening during vacuum heating at 1100°C due to loss of the protective 1.3 nm thick Conse could film remaining after 5C-2. Mosk et al. (1973) investigated the removal of inorganic contaminants, including Cu and heavy motals, from allies col polished waters by several reagent colutions (25). Using Rutherford backscattering, they concluded that SC-1/5C-2 preoxidation cleaning removes all elements heavier then Ci. Stulitur and chlorine remained after other SC1, SC-2, or other cleaning procedures at 1013/cm1. SC LSC-2 cleaning climinated Ca and Cu much more reliably than did HF-HNO. Amick (1978) reported the presence of Cl on Si after SC-2 and Safter H.SO.-H.O.; he used spark source mass spectrometric analysis (26). In 1876 Kern and Deckert published a brief review of surface contamination and semiconductor cleaning as part of a book chapter on etching (3). Murarka et al. (1977) studied methods for oxidizing Si without generating stacking faults and concluded that SC-1/SC-2 prior to exidetion is essential for this purpose (27). Gluck (1978) discussed removal of gold this purpose (27). Using (1878) discussed removal or sold from Si by a variety of solutions. The description efficiency of \$2.1 was more affective than that for \$C.2, but the revenuenced sequential treatment of \$C.1 followed by \$C.2 was found to be the most effective method at high gold surface concentrations (10 term) range (26). Peters and Deckart (1979) investigated photometry stripping by solutions chamical agents and placeme asking. The \$C.1 property chamical agents and placeme asking. vents, chamical agents, and plasmo ashing. The SC-1 procedure was the only acceptable technique by which the residues could be removed completely (29), Burkman (1981) reported on description of gold with several reagent solutions by centrifugal spraying. SCI type solution was much more effective than H.BO. H.O. while a SC4 type

alone showed poor efficiency (20).

Phillips et al. (1983) applied SIMS (secondary ion mass
spectroscopy) to determine the relative quantities of oneteminents on Si. Cleaned waters were purposely conteminated with gross quantities of numerous morganic materials and then cleaned by immercian or spray techniques ious aggressive respents including agus regia hot furning HNO, and H.SO, H.O. The Lowest residual concentrations for most impurity elements were obtained by spray cleaning with H.SO.-H.O. followed by the SC VHIP SC-2 type cleaning sequence (30). Goodman et al. (1988) demonstrated by minority carrier diffusion length massmements the effectiveness of SC-NeC-3 lot desorbing trace metals on Si (31). The author (1983) published a moview of the subject on the occasion of the Citation Clausic declaration of the original 1970-paper (32). In 1989 Watahabe et al. (33) reported dissolution rates of SiO, and Billy, films in SC-1. The rate of thermally grown SiO, in SC-1 during 20 min at 80°C was a constant 0.4 nm/min. a significant rate for sourtures with thin oxide layers. The etch rate of CVD Sign, was 0.2 nowhein under the some conditions. Measurements by the author in 1981 (and published in 1984), however, indicated much lower oxide dissolution rates under nearly identical conditions (34). Film thicknesses were measured by ellipsometry after each of four consecutive treatments in fresh 5:1:1 SC-1 at 85°C and to taled only 7.0 mm/80 min, or 0.09 mm/min. Under the same

Similar results averconditions, 5:1:1 SC-2 showed no. aging 0.13 nm/min were obtained with thermal SiO, films grown on lightly or heavily doped Si. Waters from the Si in SC-1 solutions with decreasingly lower H₂O₂ content. No stehing or strack of Si occurred until the H₂O₂ was reduced by more than 70% (34).

Bansal (1984, 1885) reported extensive results in particle removal by spray cleaning from 51 waters with SC-18C2, H.SO, H.O., and HF solution of various purity grades. He found the RCA clasning solutions to be the most effective 35, 36). Sheartman et al. (1985) described simultaneous removal of particles and contaminant films by magazonic closning with SCI solutions CD Ichiraka and Shiraki (1988) showed that atomically clean Si surfaces for MIRE can be prepared below 800°C in UHV by thermal desorption of a thin (0.5-0.5 hm), passivating exide layer that protects from C contamination (37). It is formed in a series of wet axidation (HNO, SC-1) and HF stringing steps, ter-minating with an SC-1 type treatment. Wang and Ricepson (1986) used XPS analysis to examine Si after Wet chemical treatments. RCA classing without buffered HF stripping resulted in about 30% of the Si atoms in the top 1.0 nm being oxidized, whereas with a final BHF step less than one monolayer of suboxide coverage resulted (\$9). Grundper and Jacob (1886) conducted extensive studies of 31 surfaces after treatment with SC-1/SC-2 or 5% HF solutions, using wear photoelectron and high-resolution electron energy loss spectroscopy. Oxidizing solutions produced hydrophilic surfaces, whereas HF solution led to hydrophobic surfaces consisting mainly of Si-H with some Si-CH, and Si-F (39). In 1998 Booker et al. (40) reported on decontamination by different reasons sequences. SIMS analysis was used to test for the removal of Na, K, Ca, Mg. Cr. Cu. Al. and particle impurities. The best cleaning sequence for metallics was E-SO, E-O/SC-1/SF/SC-2. Reversing the order of SC-1 and HF was most effective for particle removal and slightly less so for motal iona. Rawada et al. (1998) found by SIMS that Al an Si wafers originated from impure M.O. used in SC-2. Very high con-centrations resulted if Pyrox vestels were used in the procreating instead of fused quarte (41). In 1886 McGillivery of al (48) investigated effects of reagent contaminants on MOS capentors. Low field breakdown was more prevalent if precedution cleaning with SC-2 was terminated with HF solution instead of emitting it. No other significant disferences in electrical properties resulted from these two

Lampert (1987) examined growth and properties of oxide films on Si in verious equeous solutions, including 50-1 and 50-3 (45). Gould and Irans (1987) studied the influence of preoxidation cleaning on Si oxidation kinetics (41). They found significant rate variations depending on treatment (SC1/SC2/HF, SC1. SC2, HF, no clean). Rusyllo (1987) reported on similar experiments and found that various precordation cleans seem to affect structure and/or composition of the subsequently grown exide rether than the reactivity of the St surface (48). Shusser and MacDowell (1887) found that sub-your levels of Al in H.O. used for EC 1/SC 2 causes a substantial shift (up to 0.2V) in the fisthand voltage of a dual dielectric. Aluminum concontrates on the water surface, and basic madle such as SC-1, lead to 5 times higher levels than acid (SC-2) solutions (10). In 1667 Earn and Sahashia soci cleaning in a new chapter on wet stohing (111 Probat et al. (1986) stated that for achieving predictable diffusion from implanted doped poly-Si into single-crystal Si, an SC-1/ implanted depen poly-Si into angle-crystal al, an SC-1/ SC-2 treatment of the submrate prior to poly-Si deposition in importative (45). Exidence (1983) discussed various aspects of semiconductor cleaning, including the RCA process (13). Peterson (1983) chowed that the sequencing of cleaning solutions (H.SO_C-H₂O₂, SC-1, SC-1, HF) can have dramatic effects on particles levels (47). In 1989 herota et al. (45) reported on the contamination of SC-1/ SC-2 cleaned waters by Na, K. Al, Cr. Fe, Ni, and Cu from SC 2 cleaned waters by Na, K. Al, Cr. Fe. Ni, and Cu from solutions, showing that the absence or presence of an SiO, layer on the Si surface should affect adsorption. Description tion of Al and Fe was most effective with HF-H1O, and that

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arre authors (49) postulated of Cu and Cr with SC. that metals of high enthany, of oxide formation adsorb on the oxidized Si surface by oxide formation, whereas met als of low ionization tendency deposit electrochemically on the bare St Gould and Irane (1989) studied the eaching of native SiO, and Si in WHOH-MO. BHF. and SC-1 by ellipsometry. Savere Si curface roughness resulted from NHOH less with BHF, and none with SC-1 (50). Ohmi et al. (1989) compared particle removal efficiency of several cleaning solutions. They found that 5:1:1 SC1 effidently removes particles larger than 0.5 µm, but increases those smaller than 0.5 µm ("baze") unless the NH,OH ratio was decreased to one half or less, in which case both types of particles were reduced efficiently. However, no process ing conditions and effects of low-NH-OH SC-1 on removal of chemical contaminant films were mentioned (51). Menon & al. (1989) evaluated effects of solution chemistry (6:1:1, 50-1, DI water) and particle composition on mag-sonic cleaning efficiency at various power levels. They concluded that cleaning efficiency depends on several facters and that magneonies can pro-levels not previously strainable (12).

Alternative Cleaning Techniques

General.—Many techniques for cleaning silicon waters have been tried over the years with various degrees of success. Some techniques are useful only for specific applications or may introduce undestrable side effects. For example, glow discharge techniques (59) such as plasma ple, glow discharge techniques (59) such as plasma steining, effectively strip photocesist films but leave inotognic contominants and metals behind. Various types of sputter exching (63) can cause surface damage. Some techniques remain restricted to certain applications, such as migues remain restricted to certain applications, such as for metallization (54), or wet-chemical stehing of the silicon to remove entire surface layers by etch dissolution (3, 11). The following few techniques have been found in the ble and, in some cases, can be a desirable addition or alterious.

Brush scrupbing. Autid jet, and ultrusmic techniques.
The removal of large particles (e.g., after sawing and lapping operations) has been accomplished cines the early days with water scrubbing machines that dislodge particles hydrodynamically with brushes made of a hydrophilic material (such as nylon) while DI water or isopropy) alcohol is applied to the surface (56). A thin layer of fluid must be retained perween the brush and the waters by cureful mechanical adjustment to prevent surface amothing (23). While many contradictory claims have been made (56), if properly maintained, brush scrubbing can be very effective for removing particles larger then I am from planar and engigently hydrophilic wafer surfaces.

and preferably hydrophilic wafer surfaces.

High-pressure fluid jet disoning consists of a high-velocity jet of liquid sweeping over the surface at pressures of up to 4000 pai (55, 56). The liquid can be DI water or organic solvents. The sheet faces effectively dislodge submicron particles and penetrate into dente topography, but camege to the water can result with improperly adjusted pressure (18).

Ultragenic techniques use sonic energy of 20 kHz and above to diplodge particles. High-intensity sound waves generate pressure fluctuations that result in cavitation bubbles which upon collapsing, release enough energy to dislodge and disperse particles but can also lead to wafer damage (55). Memon et al. have recently investigated various cleaning liquids for removing particles from waferr by ultrasonic and spray jet techniques (57). Di water was best for removing polyments particles, while otherolescreame (1:1) was best (better than France) for inorganic particles. Cleaning efficiency decreased with decreasing particle size. A unique scoustical cleaning system utilizing 20 kHz frequency and only Di water as medium was introduced by Estek in 1986 (18) but has been abandoned.

Choline eleaning.—In contrast to the machanical techniques for partials removal discussed in the previous cortion, choline cleaning is a chemical treatment that removes

particles a time contaminant films but at the same time appears to and cartain contaminants to the surface. Choline, which is trimethyl-1-hydroxyethyl an monium hydroxide, was first proposed by Asame et al. ir 1978 (38) as a replacement for increased bears for exching and cleaning, it is a strong and corrective base without al call elements and etches silicon like other bases. A formulation of the chemical is available from Mallinekrod under the tradename "Summa-Clean SC-15 M." which is a dilute choine solution containing a surfactant and methanol. Exching of Si can be prevented by adding H₁O₂ as an oxidant (59). There is vary little published information on this subject most data being contained in propriatary technical reports with contradictory results. Poly-i ow engineering manufactures an automatic dual asserts apraymachine that uses a warm choline-H₂O₂-H₂O inixture and a DI water apray rinse (18). In some procedures the mixture replaces only SC-1 in the RCA cleaning procedure dure. In 1988 Kaos discussed oxide defect densities as a function of various preoxidation cleans including choline-H₂O₂-H₄O. HT-H₂O₂-H₄O.

UV come and other dry-cleaning mechanic as—Irradiating a surface with short-wavelength UV from a mercury quarts lamp in the presence of oxygen is a present tochnique for removing many contaminants. Oxygen absorbs 185 nm radiation forming very active comine as detomic oxygen (61). The technique is most suitable for oxidative removal of adsorbed organics, but is generally not effective for most inargenics or metals. Therefore, its r so in the past has been limited, in general, to special apply attors, such as GaAs water cleaning. Improvements in or ide qualities have been stained by applying the technique after SC-1/SC-2/HT-H₂O, immediately before oxidation (82). Rusyllo SC-2/HT-H₂O, immediately before oxidation (82). Rusyllo SC-1 for removing organics (83), and Koos reported improvements in properties of thermal oxide films (60).

Hosnig (1988) investigated the use of dry ic: snow for removing particles from wafers (64). Clean, liquid CO₂ from a tank is allowed to expand to form dry ice at one, which is blown across the surface. The sliding snow is quite effective for mechanically removing particles. Pa ticle detachment by electrostatic techniques has been investigated but found to be impractical (12). In 1987 FSI Corporation introduced a processing system for anhydrous i'F gas phase esching of oxide and slicate films at room temperature (68). Applications to device processing were published in 1988 (68, 67). The contamination problems i therent with IFF-Ro solutions water avoided and in combandon with UFF-Ro solutions water avoided and in combandon with the UFF-Ro solutions water avoided and in combandon with UFF-Ro solutions which we constitutes part of in ultrapure, integrated dry cleaning process that can be curied out entirely in the gas phase and may replace com antional wet techniques. Removal of installic impurities could be accomplished by use of a remote microwave plasma (68), by chlorine radical techniques (67) or by phob-induced description in reactant gases (68). These new precesses being developed are all designed to remove contaminants at low temporatures as volatile compounds without damaging the surface.

Wafer Rinsing and Drying

The last steps in wafer cleaning are rinsing and drying: both are extremely critical because clean we fire become recontaminated very easily if not process of properly. Rinsing after wet cleaning is done with flowing high-resistivity DI water, usually at room temperature (34). Magasonic rinsing is a dwarfageous (52). Contribugal apray rinsing (30) and rinsing in a closed system (23) have the advantage that the wafe is are not removed between cleaning, rinsing, and drying. Water drying after rinsing must be done by physical removal of the water rather than by allowing it to evaporate. Spin drying accomplishes this and has been the most widely used technique. Hot forced-hir drying is a preferred to hinque with less chance for particle recontamination (21, 1:2). Capillary drying is based on capillary action and surface teamine to the water. Individual waters are pulled out of DI water at 80°-85°C; less than 1% of the water remains and evaporates, leaving a particle-free surface (71). In solvent

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vapor drying wet waters are moved into the but vapor of a high-parity solvent, usually IPA (isopropy) alcoholi, which displaces the water. The waters dry quickly and are particle-free when the cassette is withdrawn above the hot vapor zone. Commercial drying systems for IPA and for nonflammable solvent mixtures are available (23, 70). The purity of the solvent is extremely important, and the water content during processing must be closely controlled. preferably by continuous recycling (51, 70).

Conclusion

Processes and techniques for cleaning, rinsing, and drying bare and oxide-coated silicon waters have been reviewed from the 1950s to the present. Wet chemical cleaning based on hydrogen peroxide solutions and implemented by sovered sochniques is still the main process used in industry. However, new wafer surface preparation technologies hased on dry processing in the gas of vapor phase are being developed that promise superior results.

A great deal of research activity is taking place in this important area of technology, as evidenced by the scheduled presentation of over 60 papers (not referenced herein) at the First International Symposium on Wafer Cleaning Technology in Semiconductor Device Manufacturing, On tober 18-18, 1989, at the Electrochemical Society Fall Mosting.

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Growth and Properties of LPCVD Titanium Nitride as a Diffusion Barrier for Silicon Device Technology

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ABSTRACT

Chemical vapor deposition has been used to deposit titanium nitride (TIN) on allicon wafers at low pressures in a cold-wall single-water reactor. Experiments are reported for pressures in the range of 180-300 maters and term executes between 460°-700°C, with titanium tetrachloride and ammonia as results. Both hydrogen and nitrogen are evaluated as diluants Deposition rates as high as 1900 Armin have been achieved. The chemical nature of the films are evaluated by Auger and Deposition, rates as high as 1900 Armin have been achieved. The chemical nature of the films are evaluated by Auger and contain the mannhology is depicted by SEM. For the most part, the films are reported. Behavior of the TIN areas quantities of exygen, chlorine, and hydrogen. Film resistivities as low as 50 million are reported. Behavior of the TIN areas quantities of exygen, chlorine, and hydrogen. Film resistivities as low as 50 million are reported. Behavior of the TIN areas quantities of exygen, chlorine, and hydrogen. Film resistivities as low as 50 million are reported. Behavior of the TIN areas quantities of exygen, chlorine, and hydrogen. Film resistivities as low as 50 million are reported by 550°C, is evaluated by measurements of contact resistance and diode lossage.

Coating of various metals with titanium ritride has been possible since the discovery in the 1920s of a chemical vapor deposition technique using electrically heated wires exposed to TiCl. $+ N_2 + H_4$ gas mixtures (1, 1). In spite of the high temperatures required (>1000 C), commercial applications for jewelry costing (3) (gold color) and tool coating (6) (west resistance) have seen considerable success. With the action of reactive physical vapor deposition techniques (5-8), where a discharge in nitrogen is created with titanium storns either evaporated or sputiared from one ejections from temberature debositions (200.C) possible and subjections of JIN costings pass persons ejections of the costings and publications of JIN costings as the persons distributed and subjections (200.C) possible and subjections of JIN costings and passible and subjections (200.C) possible and subjections of JIN costings and passible and property of the persons of dows (9, 10), and as a high temperature diffusion harrier for silicon soler cells (11, 12).

Of particular interest, in the present paper, is the application of thin TIN films to allicon device technology. Because of the concern about exposure of circuits to high temperature processes, burrier films deposited by physical vapor techniques such as low temperature reactive sput-tering (13-22) have been employed. Flowers, as integrated circuit feature siese shrink to submicron dimensions, the ability of physical techniques to uniformly coat high aspect ratio vias has become a concern. Accordingly, there has been an interest in developing a low temperature CVD has been an interest in developing a low imperature CVD process for deposition of thin films of TiN. One approach has been to explore plasma-enhanced CVD (FECVD) using TiCl, plus either nitrogen (23-26) or ammonia (27, 28). Another has been to investigate the low temperature thermal CVD process possible using TiCl, + Nid, where depositions are possible at temperatures as low as 450°C. One recent investigation has focused on a low pressure CVD process (I-PCVD) where many waters are costed at one time in a hot wall nabe reactor (28). Two others describe a LOCVD process in a cold-wall single-wafer reactor (30, 81). In this paper we elaborate on the latter approach.

Experimental

The titenium nitride depositions were carried out in a single-wafer cold-wall experimental reactor shown sche-matically in Fig. 1 (30). The chamber was stainless resi and enclosed a water and air-cooled lamp accombly used to hear the water. A single 10 kW tungsten helogen lamp was employed that can heat a 4 in. wafe : to 700°C ?apidly A load lock was used to maintain an ox) gen and water va por free deposition environment.

Reactive gener were introduced through a showerhead gas distributor several inches above the water. The TiCl and NH, were introduced through two separate lines and mixed for the first time in the shower head. As long as these two cases are mixed close to the hot water on which the depact is to be made, the formation of NH.Cl can be avoided as has been demonstrated in another experimen similar to this one (81).

Before beginning TiCl, or NH, flows, a nitrogen flow was reablished in the TiCl, line downstream of the TiCl, bot ortableaned in the field line downstream or the field son the. Next the Field flow was instanted and sites it was stabilized then the NH, flow was introduced. This proce dure kept TiCl, and NH, from mixing it the TiCl, line are causing solid deposits there.

All of the gases were introduced through mass flow controllers (BCFCs), including the TICL valor which was of tained by heating TICL liquid to 40°C. The TICL line wa heated to 50°C to prevent any condens tion of this vapor. Since the pressure of the TiCL vapor at 40°C was only 5 torr, we calibrated our Unit MFC (UFC 100) by measuring the time it took for a specified altrogen mass flow (sug-plied at 40 terr) to increase the pressure in our chambs from 160 to 200 mitors. We then repeated this measuremen when the nitrogen was supplied at 10 ; at By this metho

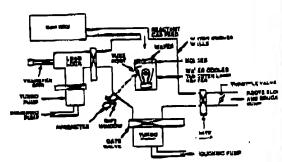


Fig. 1. Schematic of CVD reach system

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